

Emerging Bioreactor Research in Iowa: Design and Performance

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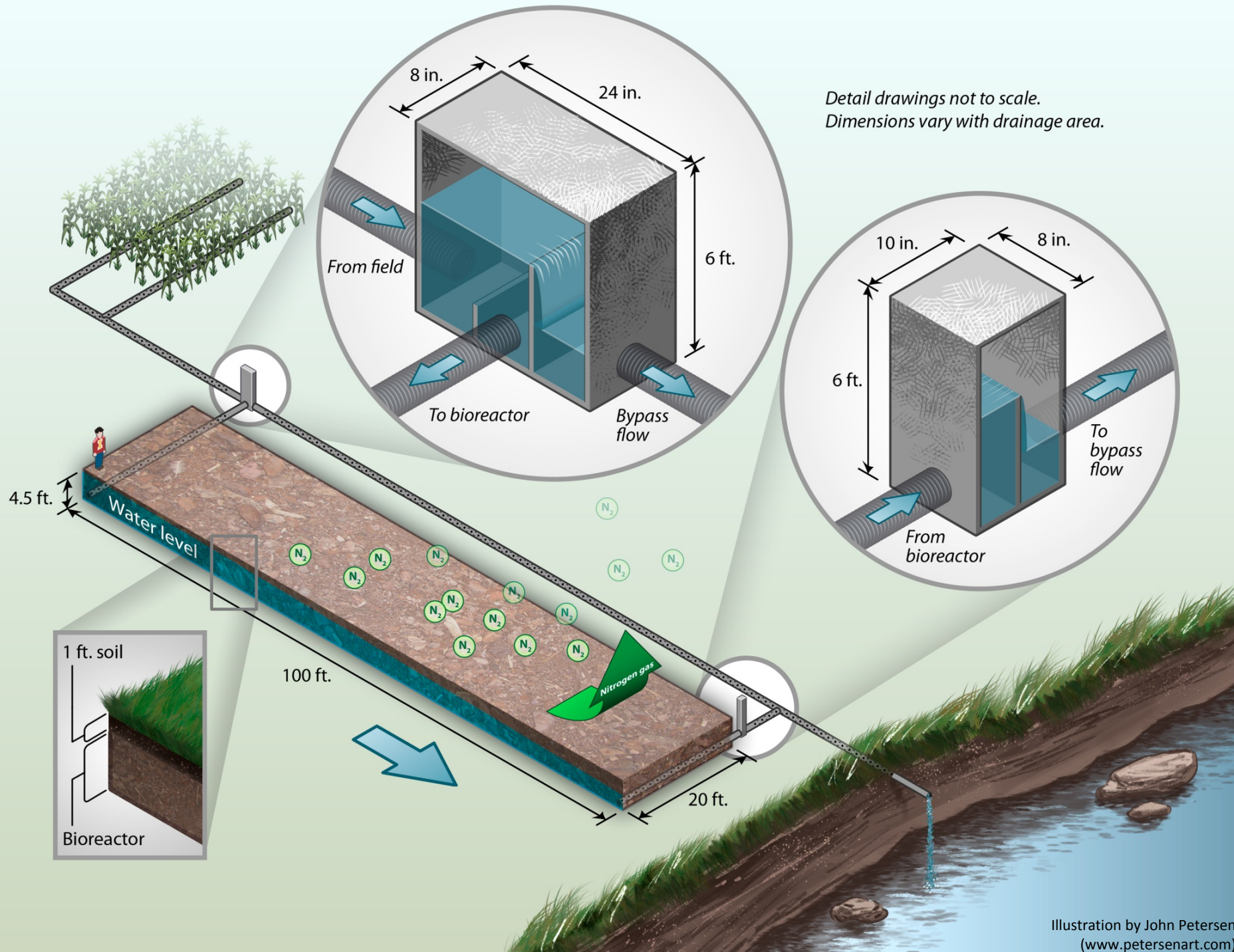
Agricultural & Biosystems Engineering

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Design Model User Interface

Subsurface Drainage Bioreactor Design

Developed by M. Helmers and L. Christianson, ABE Iowa State University

Instructions: Enter values in gray cells

| Field Information: | |
|--|--------------|
| Tile Size (in) | 7.7386 |
| Tile Grade (%) | 1 |
| Dual Wall | no |
| Velocity in Pipe (ft/s) | 2.94 |
| Peak Flow from Tile Size (cfs) | 0.9611 |
| Media Information: | |
| Conductivity of Wood Media (ft/s) (K) | 0.31168 |
| Porosity of Wood (ρ) | 0.7 |
| Bioreactor Inputs and Calculations: | |
| Flow Length (ft) (L) | 80 |
| Trench Width (ft) (W) | 33 |
| Inlet height (ft) | 2 |
| Outlet height (ft) | 1 |
| Head Drop (ft) (ΔH) | 1 |
| Flow Depth (ft) (d) | 1.5 |
| Hydraulic Gradient (i) | 0.0125 |
| Results: | |
| Bioreactor Flow Rate (cfs) (Q) | 0.19 |
| Hydraulic Retention Time (hours) (HRT) | 3.99 |
| % of peak flow that can be passed through bioreactor | 20.07 |

Explanatory Notes:

Known from site

Known from site

no

Mannings Gravity Driven Flow Equation = $1.49 \times \sqrt{\left(\frac{\text{Tile Grade}}{100}\right)} \times \frac{\left(\frac{\text{Tile Size}}{\text{(Conversion)}}\right)^{\frac{2}{3}}}{0.012(\text{for dual wall})\text{OR } 0.015(\text{for non-dual walled})}$
 Flow rate = Velocity x Area of Tile

Converted from 9.5 cm/s to ft/s; value determined in Porous Media Lab, ABE-ISU

Taken from van Driel et al., 2006

Iteratively choose

Iteratively choose

Iteratively choose

Iteratively choose

Calculated based on difference between inlet and outlet

Calculated to be in bioreactor middle (average of inlet and outlet height)

Head Drop / Flow Length

Darcy's Law for Porous Media Flow = $Hvd \cdot \text{Conductivity} \times \text{Hyd. Gradient} \times \text{Flow Area} = KiA = Ki(W \times d)$

$HRT = \tau = \frac{\text{Volume} \times \text{porosity}}{\text{Flow rate}} = \frac{V\rho}{Q} = \frac{l \times w \times d \times \rho}{Q}$ (conversions included)

Bioreactor Flow Rate / Peak Flow from Tile

Bioreactors are designed to treat approximately 20% of the peak flow rate.

The design retention time is between 4 - 8 hours (Robertson et al., 2000; van Driel et al., 2006; Christianson

Three Sites in Iowa

Northeast Research Farm - NERF (Nashua)

Installed April 2009

14.2 ha drainage area

36.6 x 4.6 x 1.0 m



Three Sites in Iowa

Greene Co.

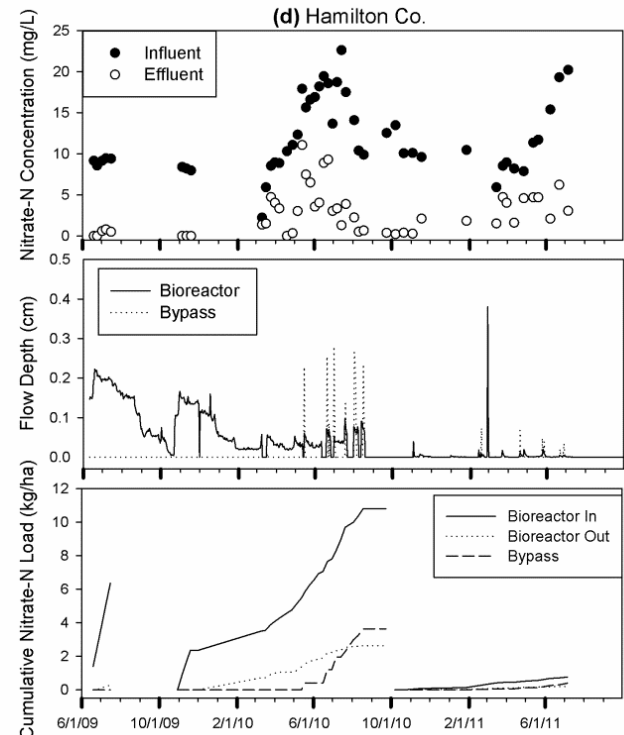
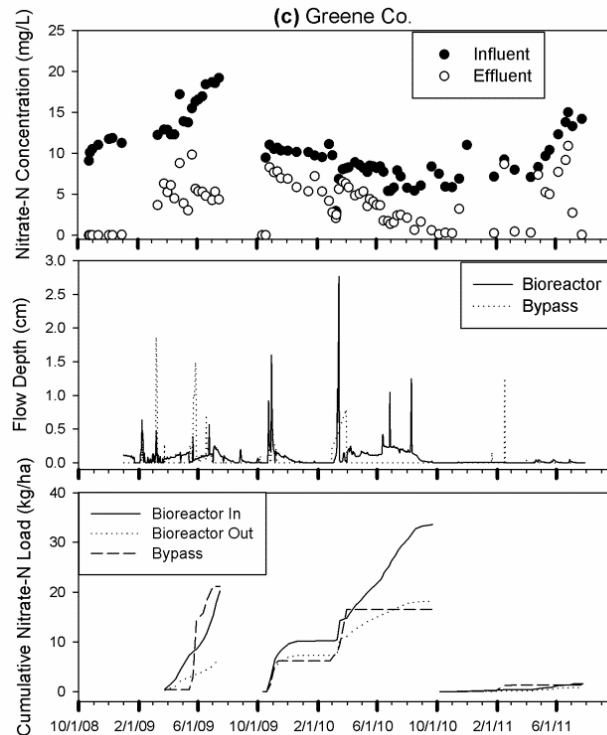
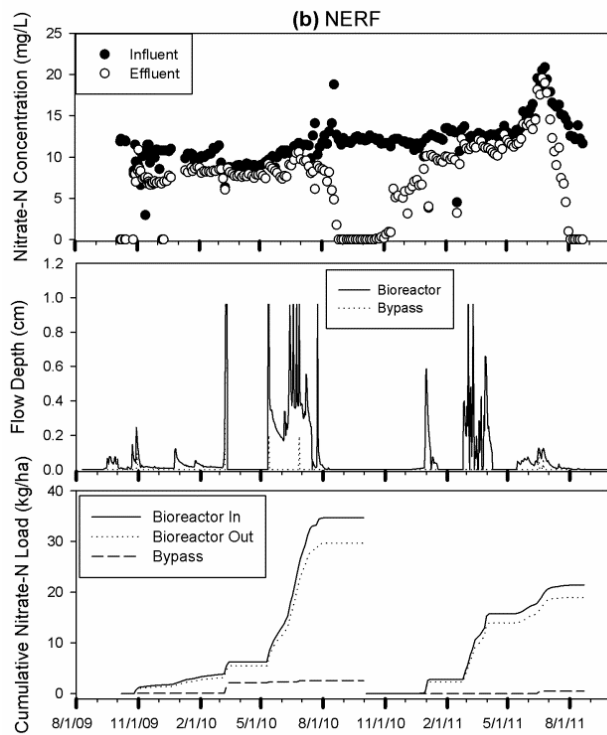
Installed Aug. 2008
19 ha drainage area
15.2 x 7.6 x 1.1 m



Hamilton Co.

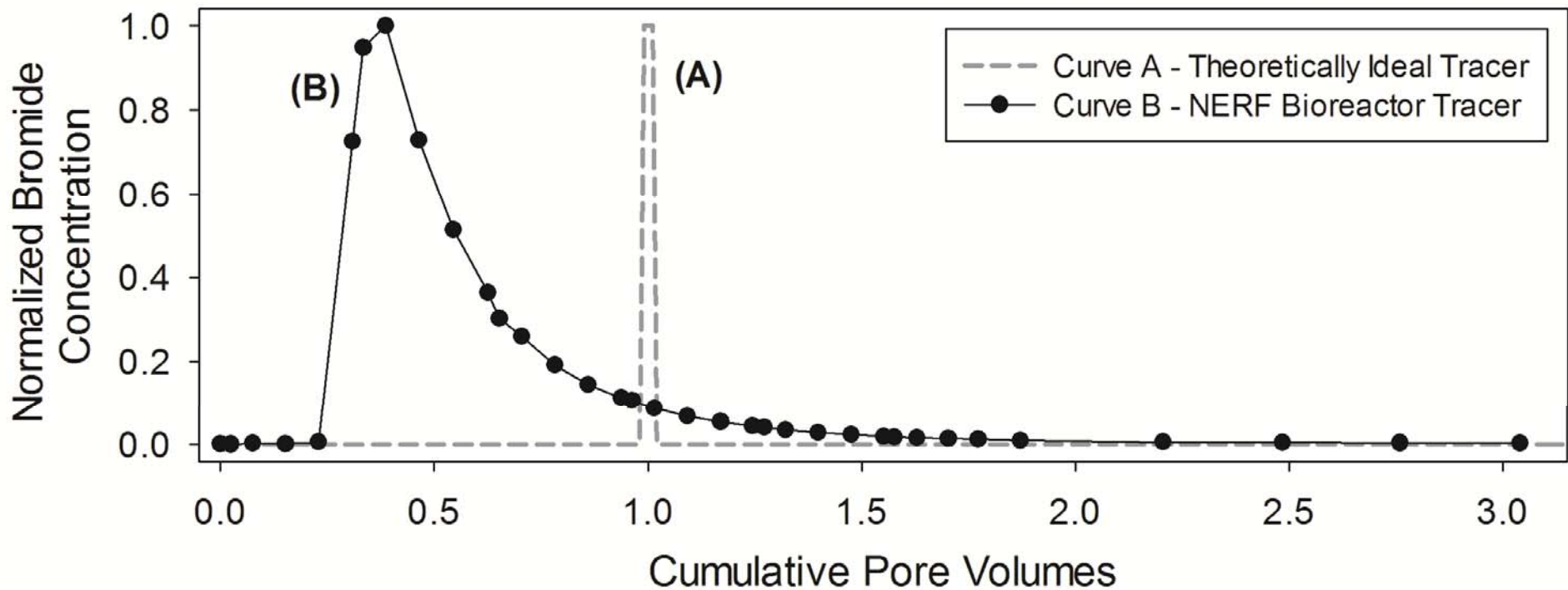
Installed June 2009
20.2 ha drainage area
30.5 x 3.7 x 0.9 m





| | | | |
|---------------------------------------|-----------|-----------|-----------|
| Mean annual total load reduction | 12%-14% | 27%-33% | 49%-57% |
| Load removed (kg N/ha) | 2.5-5.1 | 0.8-15.5 | 0.6-8.1 |
| Percent of water treated | 91%-99% | 51%-68% | 73%-87% |
| Removal Rate (g N/m ³ /dy) | 0.86-1.56 | 0.41-7.76 | 0.42-5.02 |

NERF Bioreactor Design Evaluation



Tracer Residence Time: 3.5 hrs
Theoretical Retention Time: 6.3 hrs
Effective Volume (e): 0.55
Hydraulic Efficiency (λ): 0.40

Effective plug flow, but ineffective utilization of flow volume

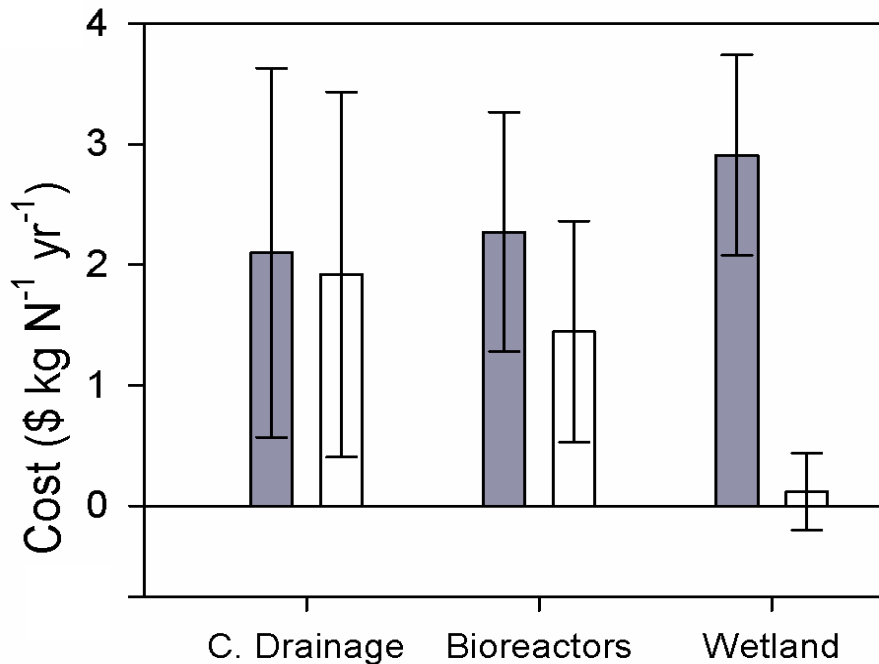
What do bioreactors cost?

| | Structure | Contractor | Woodchips | Supplies | Total | \$ total/ha drained |
|--------------|------------|------------|------------|----------|-------------|---------------------|
| Greene Co. | \$2,750.00 | \$5,250.00 | \$1,245.00 | \$500.00 | \$9,745.00 | \$512.35 |
| Hamilton Co. | \$1,640.00 | NA† | \$2,400.00 | \$350.00 | \$4,390.00 | \$216.96 |
| Iowa 1 | \$1,970.00 | \$1,800.00 | \$3,350.00 | \$560.00 | \$7,680.00 | \$316.30 |
| Iowa 2 | \$1,270.00 | \$1,890.00 | \$3,000.00 | \$780.00 | \$6,940.00 | \$428.73 |
| Iowa 3 | \$1,640.00 | \$5,030.00 | \$4,650.00 | \$500.00 | \$11,820.00 | \$194.72 |
| Iowa 4 | \$1,480.00 | \$2,710.00 | \$2,520.00 | \$400.00 | \$7,110.00 | \$585.64 |

†contractor time donated

Range: \$78.80/ac to \$237.00/ac

Average: \$152.07/ac



**Amortized Drainage BMP Costs
over 50 years:
Installation, Maintenance, Replacement**

N-Based Equalized Annual Cost (EAC)
 N-Based EAC with Government Payment

4% real discount rate

Acknowledgements

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- Project number: GNC09-103 from the USDA Sustainable Agriculture Research and Education North Central Region Graduate Student Grant Program.

Do the woodchips matter?

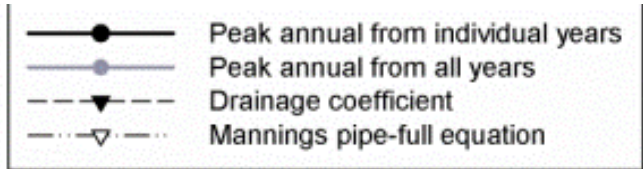
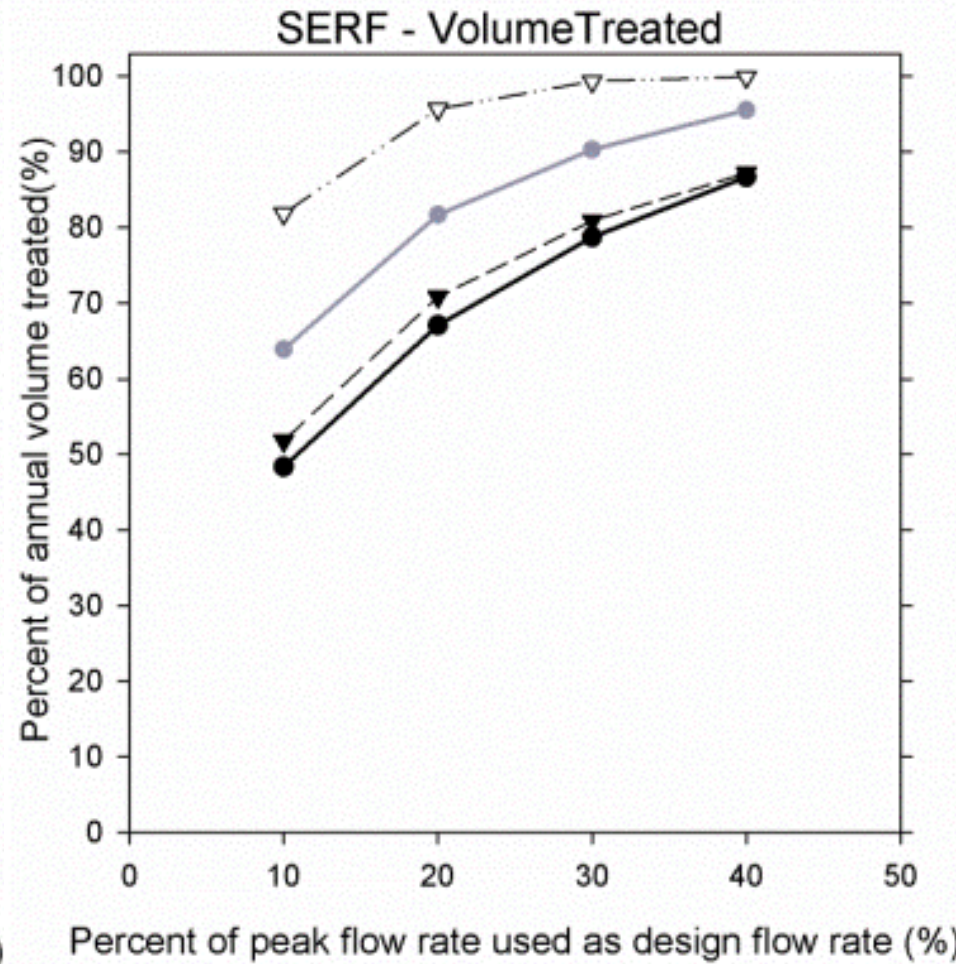
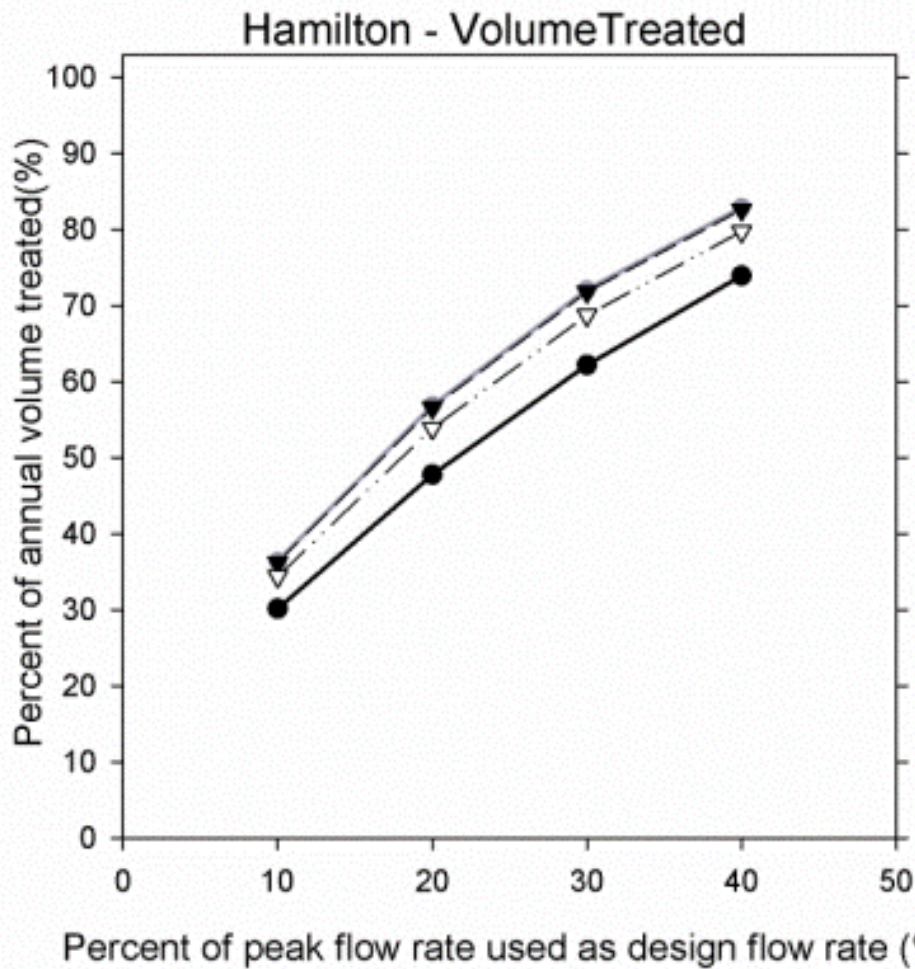


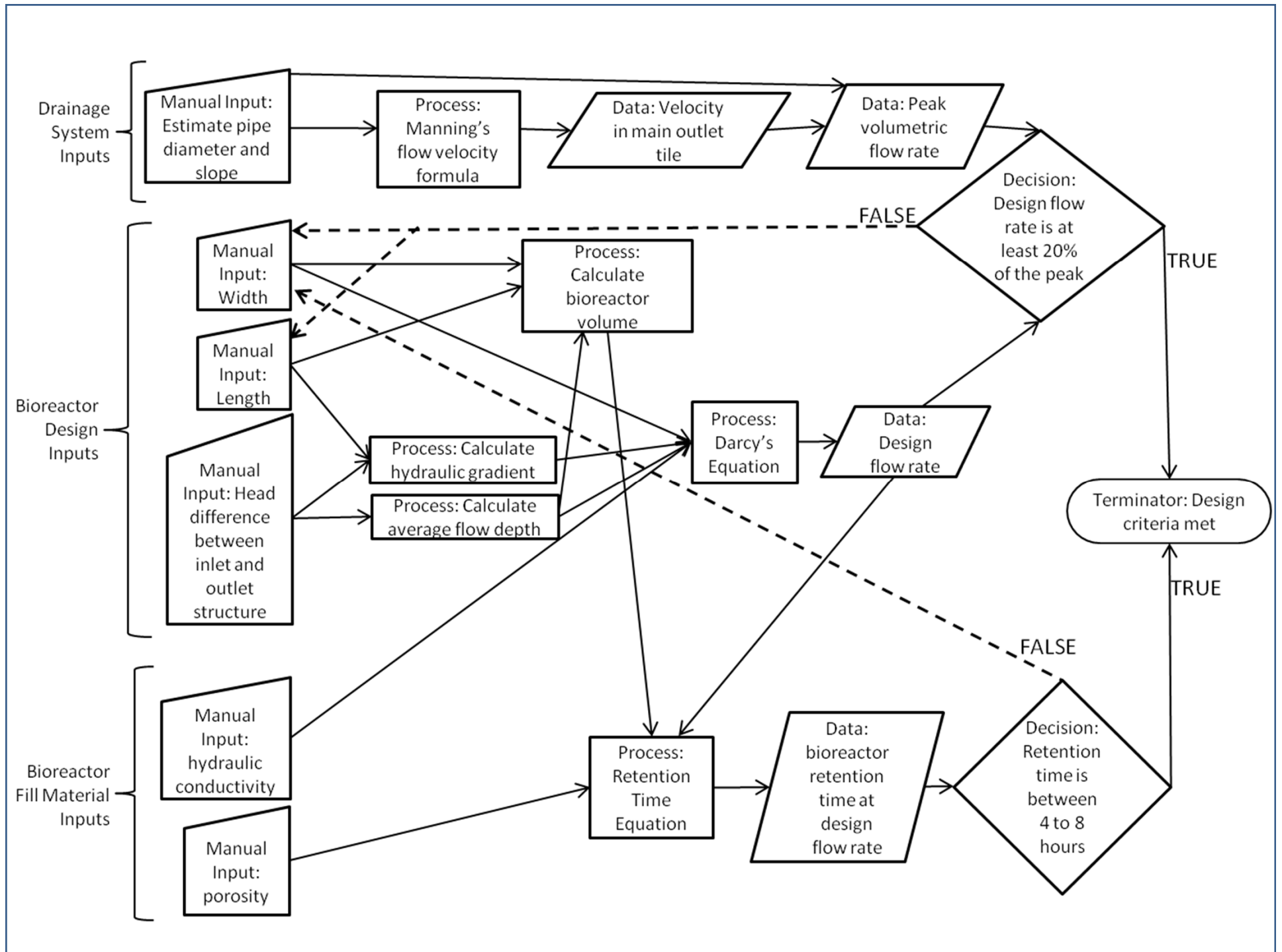
“Good” Chips
Better uniformity and
consistent piece size



“Bad” Chips

| | Area | D Coeffici | Tile Dia (in) | Slope (%) | cfs Mannings | cfs D coefficient | Notes |
|----------|-------|------------|---------------|-----------|--------------|-------------------|--|
| SERF | 27 | 0.75 | 12 | 0.74 | 2.66 | 0.85 | coefficient calculated from flow data, single wall tile; slope from Reid (Google maps) |
| Hamilton | 38.25 | 0.5 | 8 | 0.5 | 0.74 | 0.80 | "very small slope", single wall tile |



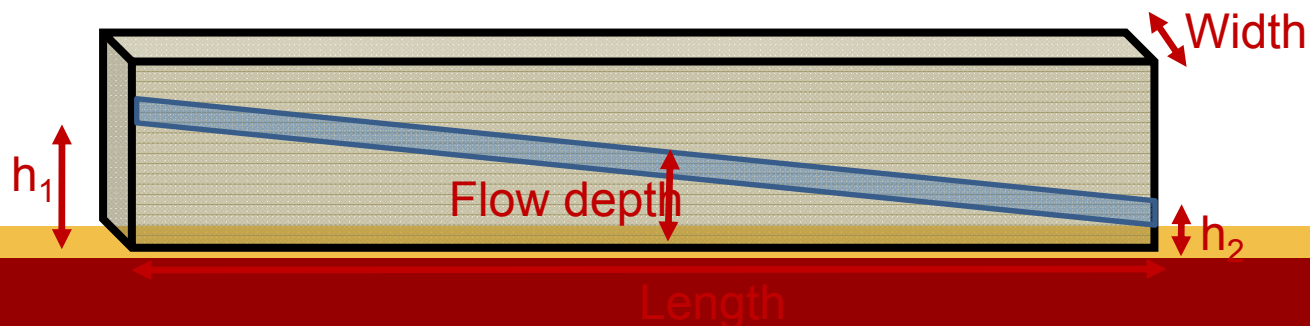


Darcy's Equation: Flow Through Porous Media

$$Q = KiA$$

What % of the peak flow rate do these bioreactor dimensions allow?

- Q: Volumetric Flow Rate (m³/sec)
- K: Hydraulic Conductivity (cm/sec):
 - 0.35-1.6 cm/sec for sawdust to 61 mm chips (Cameron & Schipper 2010)
 - Hardwood chips commonly used in lowa bioreactors = 9.5 cm/sec
 - Can change over time
- i: Hydraulic Gradient (m/m), head drop divided by the bioreactor length
- A: Cross-sectional Area (m²)



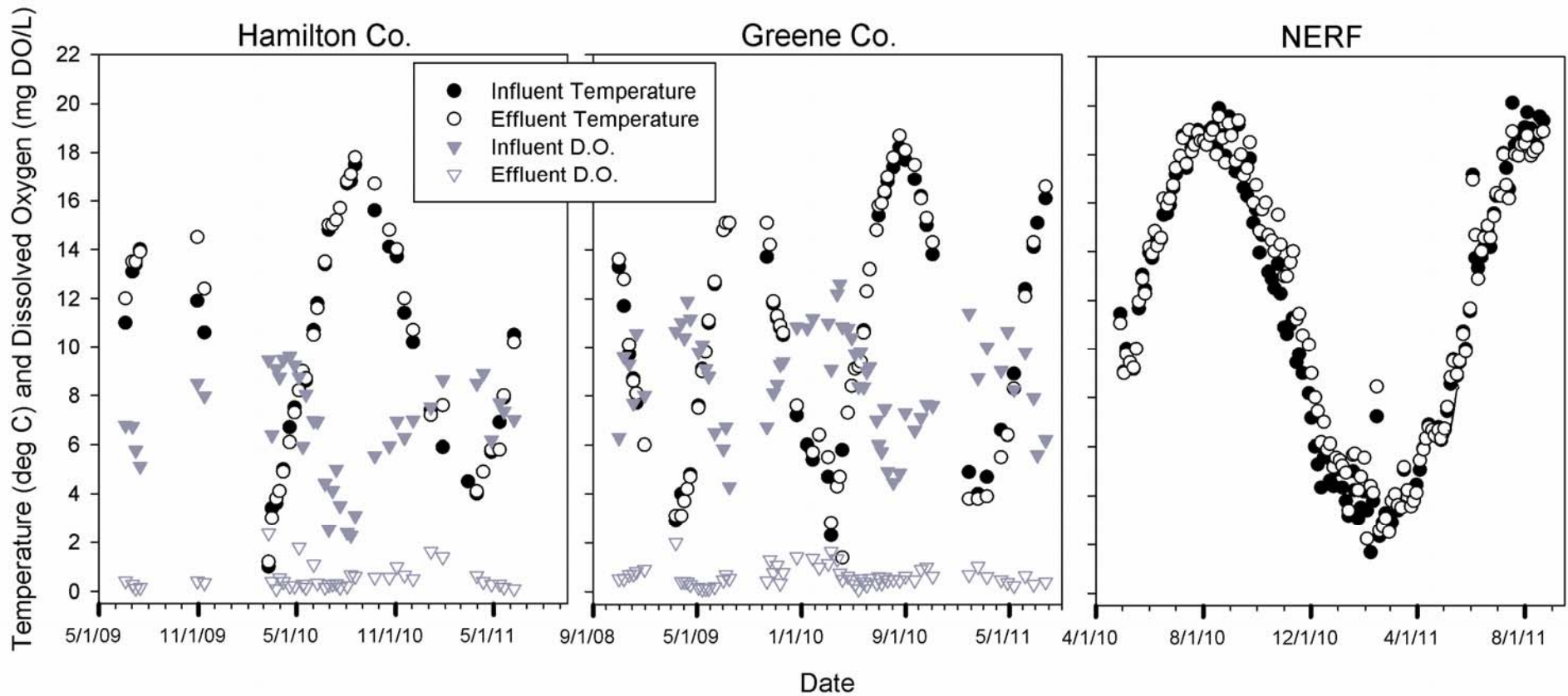
Retention Time Equation

$$\tau = \frac{\rho V}{Q}$$

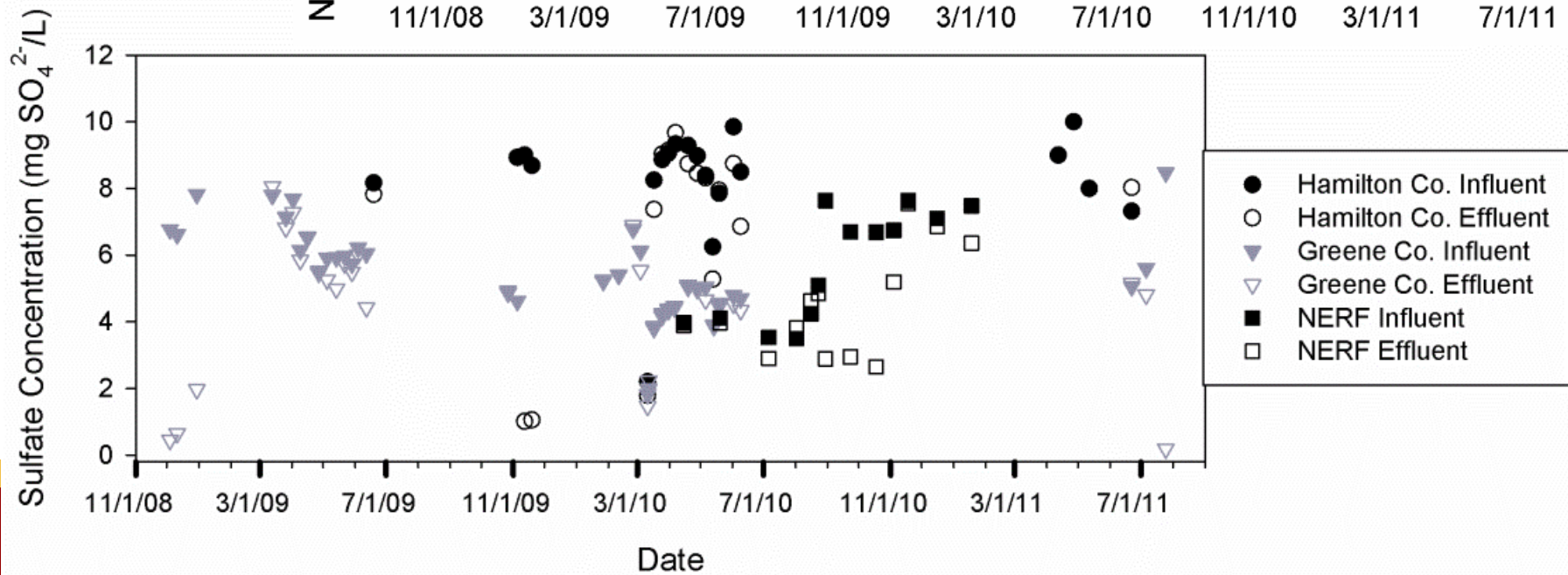
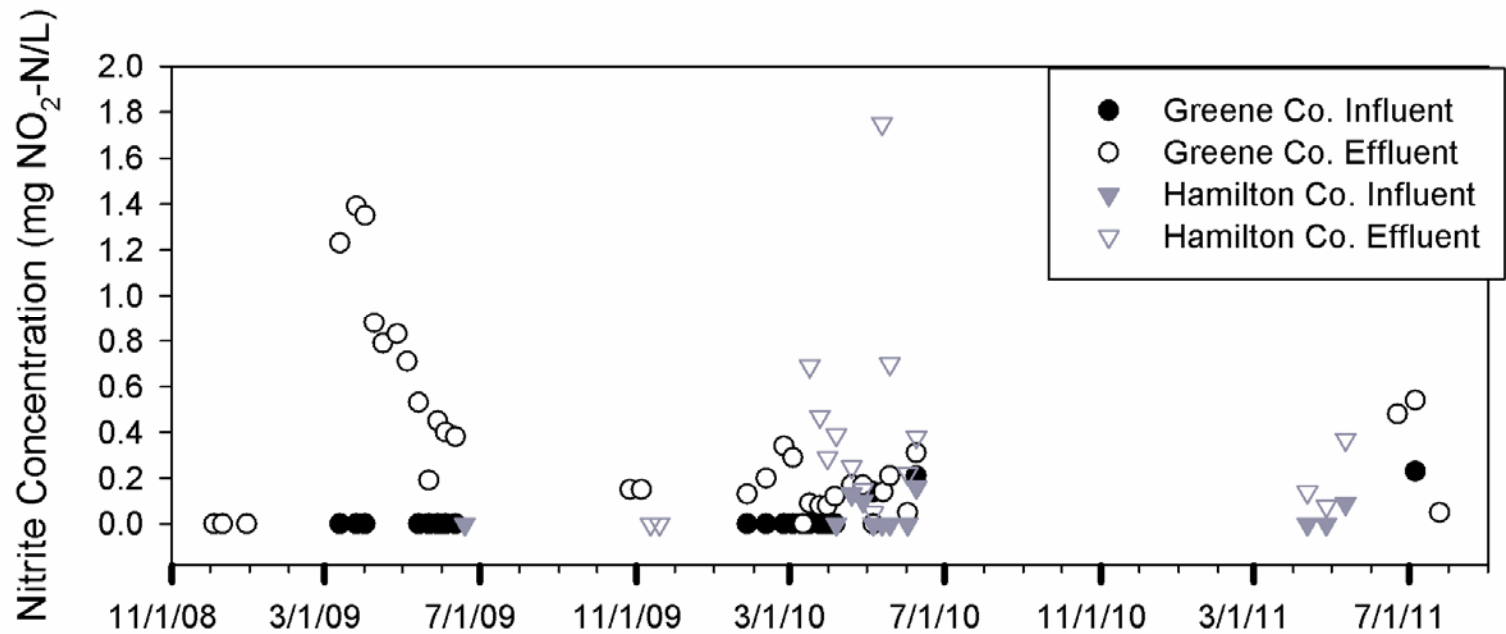
What retention time do these bioreactor dimensions allow?

- τ : Retention Time
- V : Bioreactor Volume (m^3)
 - Depth of the bioreactor is set by the tile depth, but use average flow depth for volume.
- ρ : Porosity, range for woodchips: 0.63-0.86
 - Packing density, moisture content, chip size, and chip age
- Q : Flow rate (m^3/sec), Calculated from Darcy's equation
- Is a function of Length:
$$\tau = \frac{\rho V}{KiA} = \frac{\rho(l \times w \times d)}{Ki(w \times d)} = \frac{\rho l}{Ki}$$

Temperature and Dissolved Oxygen



Chapter 4: Nitrite and Sulfate

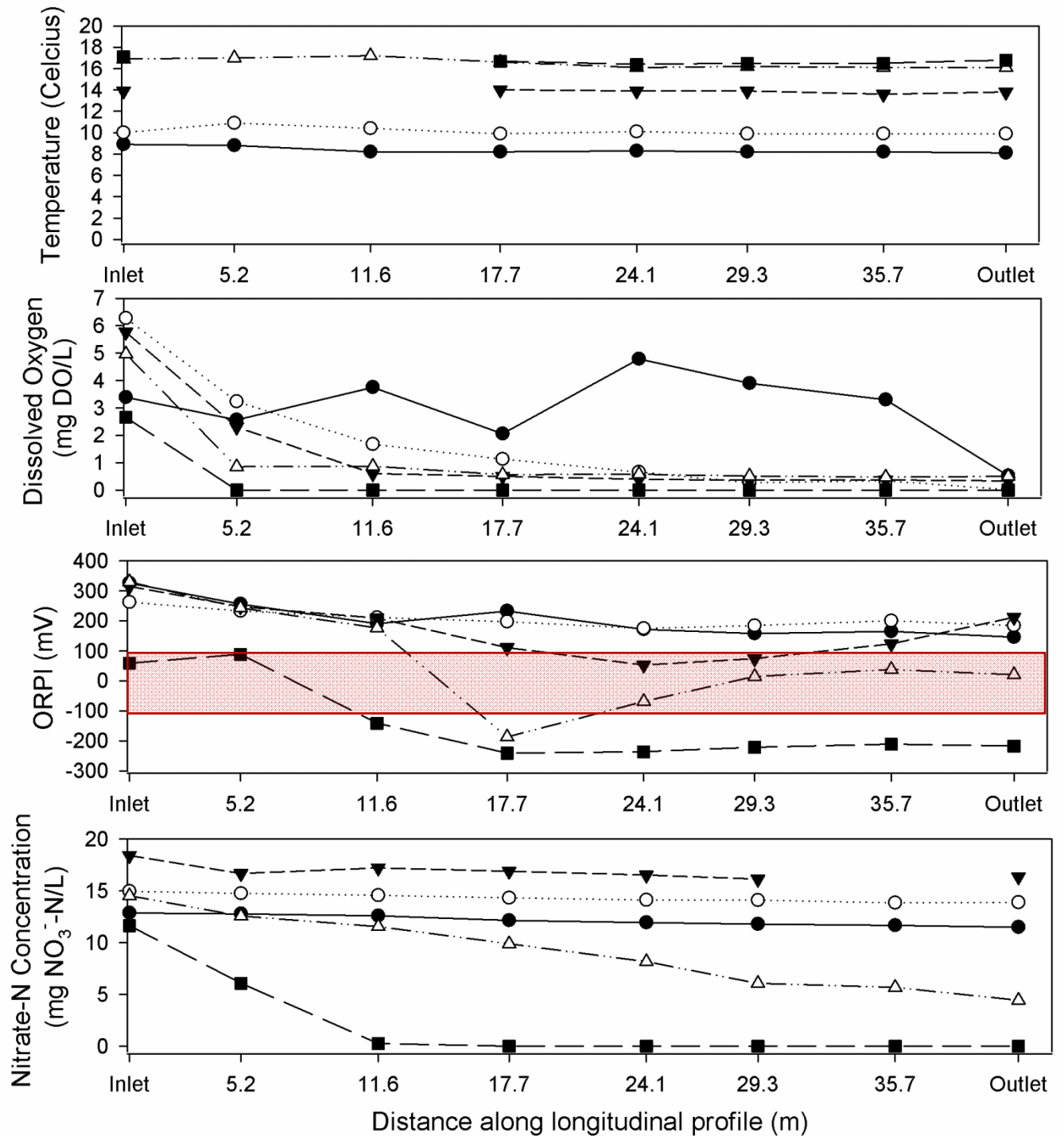
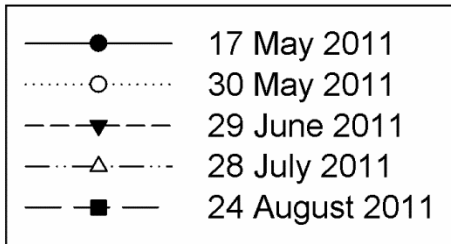


Bioreactor Monitoring

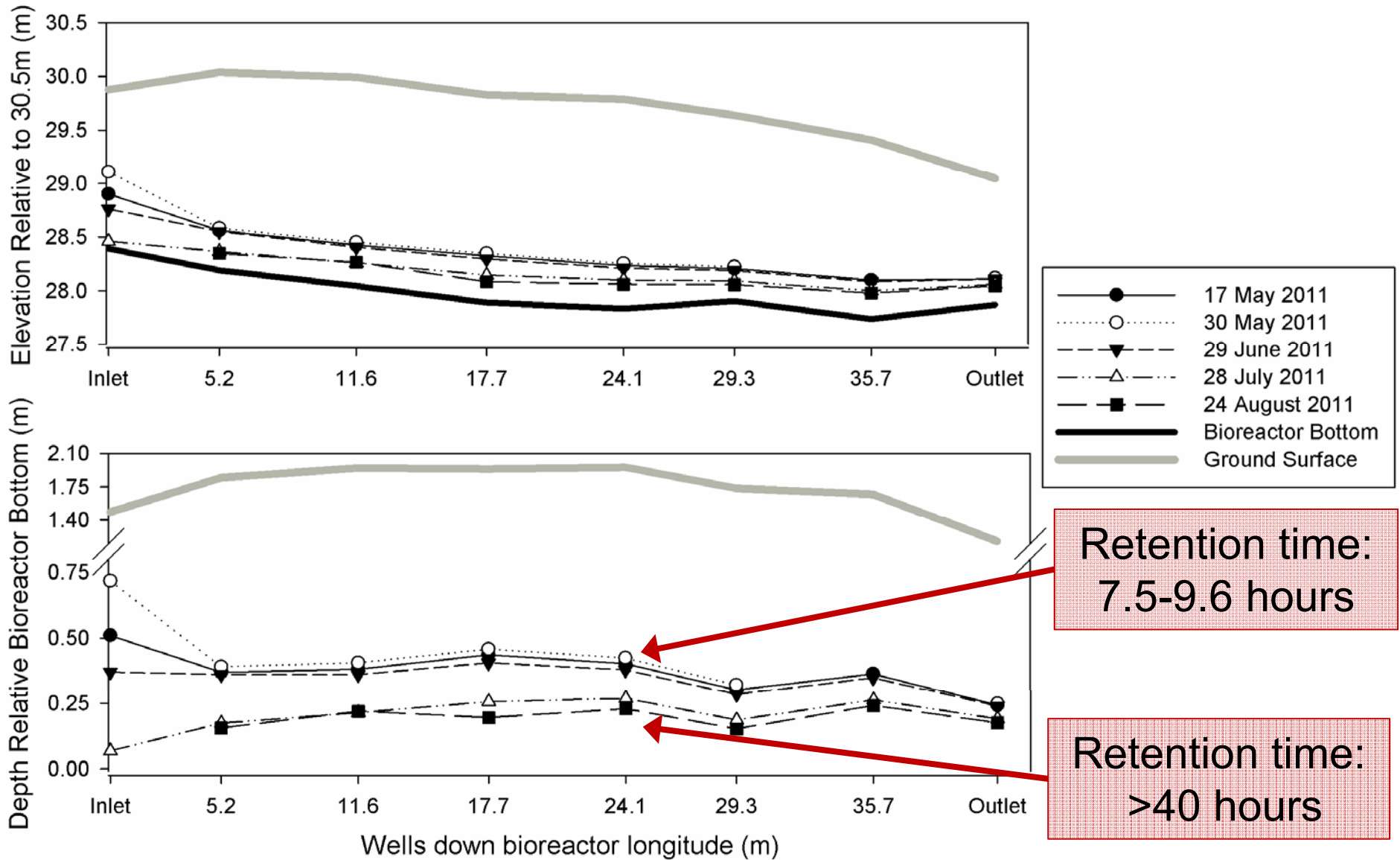
- Inflow and outflow
 - Nitrate-N
 - Flow rate
- Well sampling
 - Temperature
 - Dissolved oxygen
 - Oxidation reduction potential (ORP)
 - Nitrate-N
 - Flow depth (continuous)
- Tracer testing



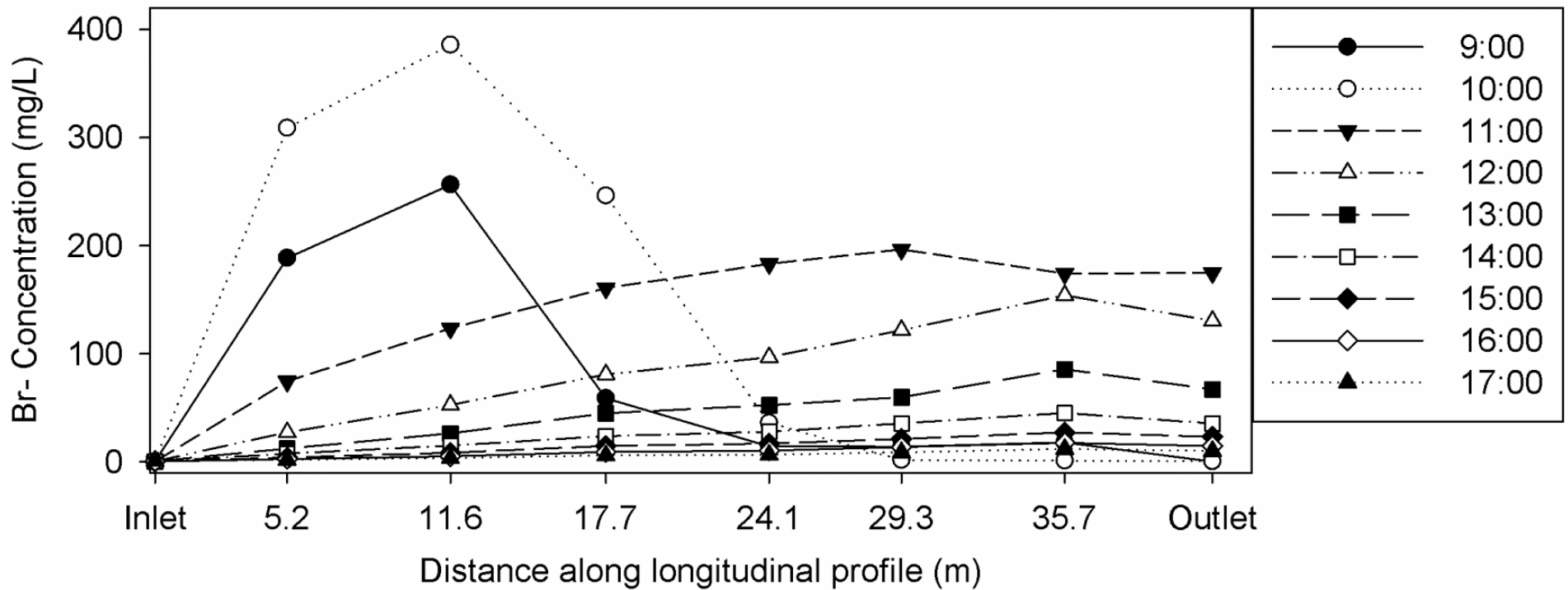
Bioreactor Internal Performance



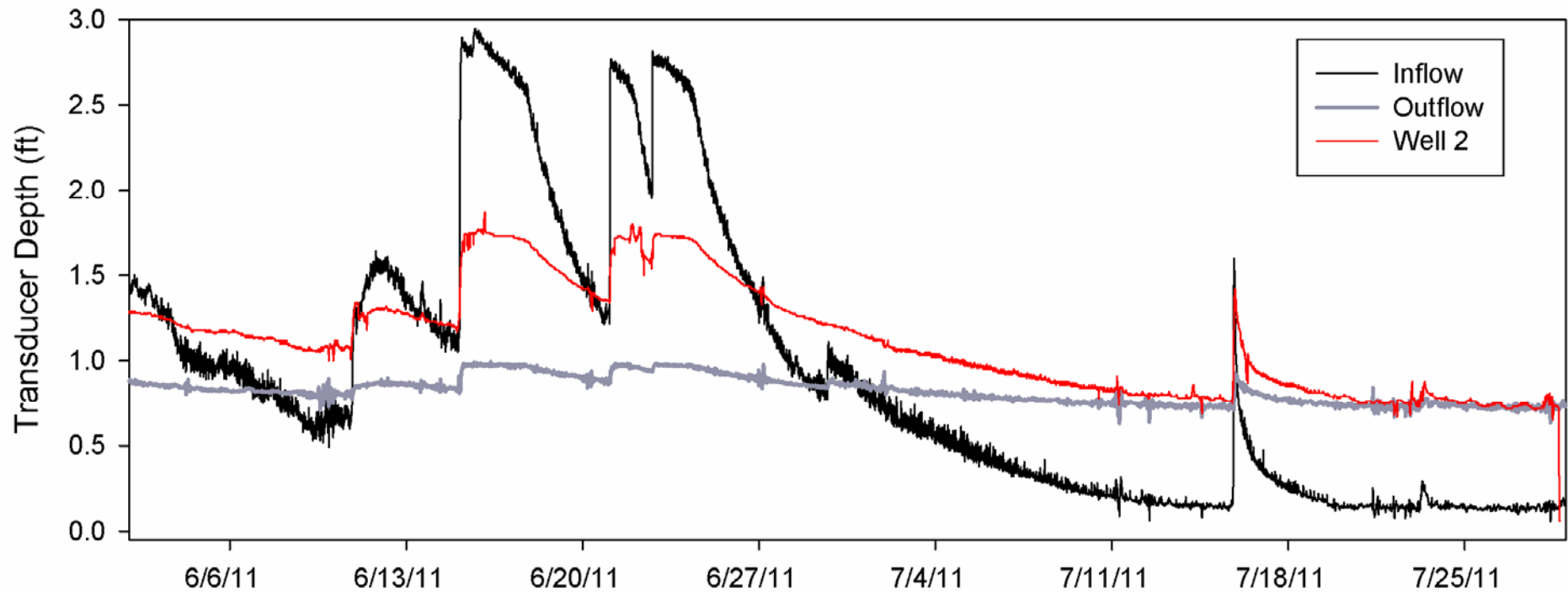
Bioreactor Water Depths



Bioreactor Internal Performance: Tracer Testing



Bioreactor Internal Performance: Hydrograph Progression

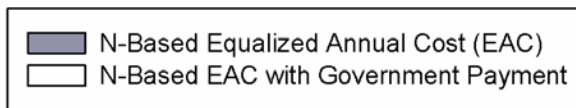
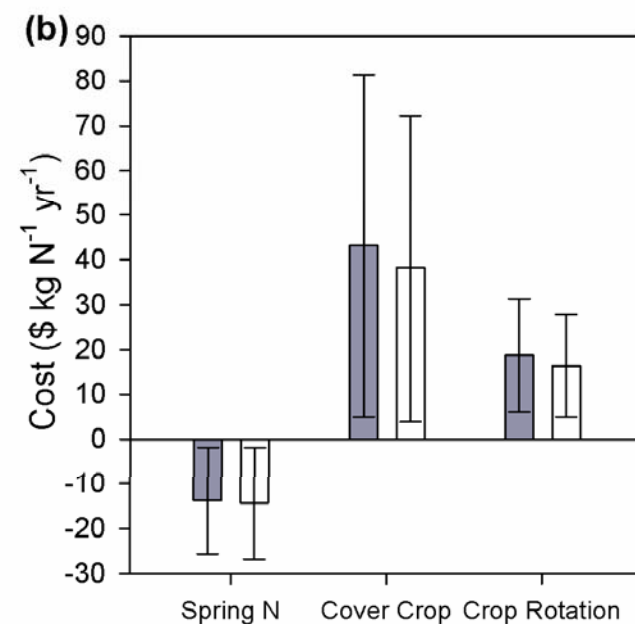
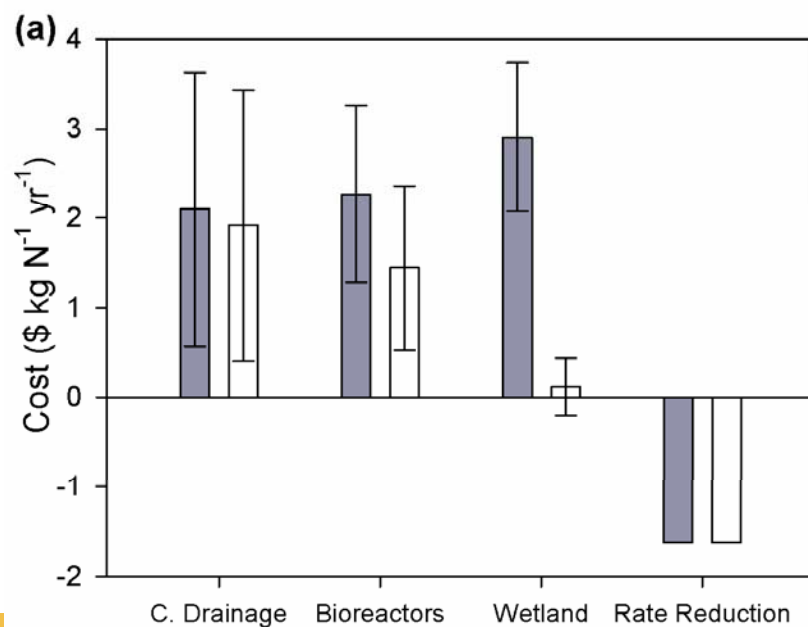
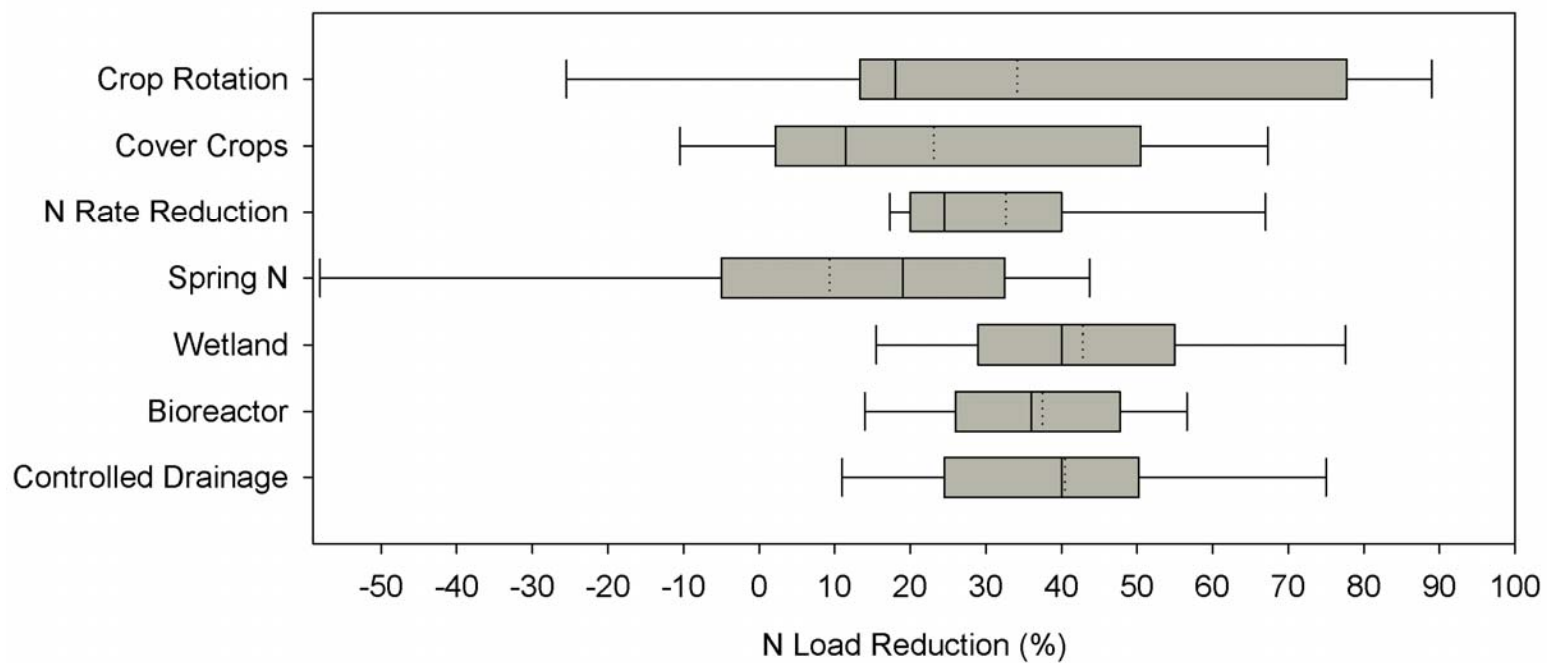


Chapter 4: Bioreactor Load Reduction

| | Water Year | Bio. In (kg N/ha) | Bio. Out (kg N/ha) | Mean Bio. Reduction % [‡] | Removal Rate (g/m ³ /dy) |
|------------|-------------------------|----------------------|-----------------------|---------------------------------------|--|
| Pekin | 2004-2005 | 5.0 | 2.8 | 43.7 | 1.07 |
| | 2005-2006 | 1.2 | 0.7 | 43.5 | 0.75 |
| | 2006-2007 | 33.6 | 21.1 | 37.4 | 3.78 |
| | 2007-2008 | 14.8 | 8.4 | 43.8 | 2.53 |
| | 2008-2009 | 7.1 | 5.0 | 29.1 | 0.57 |
| | 2009-2010 | 7.4 | 5.8 | 22.0 | 0.67 |
| | 2010-2011 | 2.0 | 0.5 | 74.0 | 0.38 |
| NERF | 2009-2010 | 34.7 | 29.7 | 14.6 | 1.56 |
| | 2010-2011 [¶] | 21.4 | 18.9 | 11.7 | 0.86 |
| Greene Co. | 2008-2009 [#] | 20.2 | 6.5 | 68.0 | 7.76 |
| | 2009-2010 | 33.6 | 18.1 | 46.0 | 6.69 |
| | 2010-2011 ^{††} | 1.6 | 0.8 | 50.4 | 0.41 |
| Hamilton | 2009-2010 | 10.8 | 2.6 | 75.7 | 5.02 |
| Co. | 2010-2011 ^{‡‡} | 0.8 | 0.2 | 73.9 | 0.42 |

Chapter 4: Total Load Reduction

| | Water Year | Total In (kg N/ha) | Total Out (kg N/ha) | Mean Total Reduction %‡ |
|--------------|------------------------|-----------------------|------------------------|----------------------------|
| Pekin | 2004-2005 | | | |
| | 2005-2006 | | | |
| | 2006-2007 | | | |
| | 2007-2008 | | NA ^{§§} | |
| | 2008-2009 | | | |
| | 2009-2010 | | | |
| | 2010-2011 | | | |
| NERF | 2009-2010 | 37.3 | 32.2 | 13.6 |
| | 2010-2011¶ | 21.9 | 19.4 | 11.5 |
| Greene Co. | 2008-2009 [#] | 41.4 | 27.6 | 33.3 |
| | 2009-2010 | 50.1 | 34.6 | 30.9 |
| | 2010-2011†† | 2.9 | 2.1 | 27.3 |
| Hamilton Co. | 2009-2010 | 14.4 | 6.3 | 56.6 |
| | 2010-2011‡‡ | 1.2 | 0.6 | 48.6 |



| Item | Cost Timing | Minimum cost | Mean cost \$ ha ⁻¹ | Maximum cost | Notes | Reference |
|--|---------------------------|-----------------|----------------------------------|-----------------|---|--|
| Both control structures | yx 1 | \$49.42 | | \$197.68 | Two control structures at \$500 to \$2000 ea.; 20.2 ha treatment area | Agri Drain Corp, personal comm., 2011 |
| Structure transport | --- | | | | Assumed included above | Assumption |
| Woodchip cost | 1 | | \$116.14 | | Two semi loads at \$975 chips + \$200 transport ea.; 20.2 ha treatment area | ISA, personal comm., 2011 |
| Woodchip transport to farm | --- | | | | Included above | |
| Design cost | 1 | \$0.00 | | \$31.63 | Assumed: \$40 h ⁻¹ for 2 days of work or NRCS service provider; 20.2 ha treatment area | Assumption |
| Contractor fees | 1 | \$27.68 | \$60.61 | \$98.84 | Back hoeing at \$35.00 h ⁻¹ , \$76.65 h ⁻¹ , \$125.00 h ⁻¹ for 16 hours to treat 20.2 ha | ISU Extension, 2010; Assumptions |
| Seeding bioreactor surface | 1 | \$0.05 | \$0.11 | \$0.15 | Seeding grass, broadcast with tractor; for 20.2 ha treatment and 0.10 ha bioreactor at \$9.88, \$22.61, and \$29.65 per ha | ISU Extension, 2010 |
| Seed cost | 1 | | \$1.11 | | Seed costs from dealer: \$222.27 ha ⁻¹ for CRP Mix (CP23) Diversified mix; bioreactor surface 0.005 of treatment area | Prairie Land Management: http://www.habitatnow.com/store/shop/shop.php?pn_selected_category=37 |
| Misc. materials | 1 | | \$8.80 | | 6" tile \$890 per 305 m(1000 ft); Assume 61 m needed for control structure connections for 20.20 ha treatment area | Agri Drain Corp, personal comm., 2011 |
| Total cost of establishment | | \$203.19 | | \$454.35 | TPVC | |
| Time to raise/lower | 1-n | \$1.19 | | \$2.97 | Three hours per yx with farm labor wages at \$8-\$20 h ⁻¹ , 20.20 ha treatment area | Assumption; ISU Extension, 2010 |
| Mowing/maintenance | 1-n | \$0.12 | | \$0.62 | Spot mowing bioreactor at \$24.71 to \$123.55 ha ⁻¹ for 20.2 ha treatment | ISU Extension, 2009 |
| Total cost of establishment and maintenance | | \$231.33 | | \$531.32 | TPVC | |
| Replacement yx 20 | 20 | \$65.66 | | \$98.18 | Single sum TPVC at 20 years: woodchips, contractor, seeding | |
| Replacement yx 40 | 40 | \$40.26 | | \$85.98 | Single sum TPVC at 40 years: woodchips, contractor, structures, seeding | |
| Gate replacement | 8, 16, 24 _{xxxx} | | \$16.76 | | Summation of single sum TPV every 8 years for 5 gates per structure (\$14.17 to \$15.32 per ea. for 15 cm structure) 2 structures per 20.2 ha | Agri Drain Corp, personal comm., 2011 |
| Total cost of establishment, maintenance, and replacement | | \$354.01 | | \$732.25 | TPVC | |